

(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property Organization  
International Bureau(43) International Publication Date  
2 March 2006 (02.03.2006)

PCT

(10) International Publication Number  
**WO 2006/021796 A1**(51) International Patent Classification<sup>7</sup>:  
C02F 1/06

B01D 3/06,

(81) Designated States (unless otherwise indicated, for every kind of national protection available): AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BW, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, EG, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KM, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NA, NG, NI, NO, NZ, OM, PG, PH, PL, PT, RO, RU, SC, SD, SE, SG, SK, SL, SM, SY, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, YU, ZA, ZM, ZW.

(21) International Application Number:  
PCT/GB2005/003329

(22) International Filing Date: 26 August 2005 (26.08.2005)

(25) Filing Language: English

(26) Publication Language: English

(30) Priority Data:  
0419117.7 27 August 2004 (27.08.2004) GB

(71) Applicant (for all designated States except US): O.H.D.L. OPTIMISED HYBRID DESALINATION LIMITED (GB/GB); 71 Kingsway, London WC2B 6ST (GB).

(72) Inventors; and

(75) Inventors/Applicants (for US only): AWERBUCH, Leon [US/US]; 17 Trinity Road, Winchester, MA 01890 (US). SOMMARIVA, Corrado [IT/AE]; MoH MacDonald, P.O. Box 47094, Abu Dhabi (AE).

(74) Agent: HILLIER, Peter; Marks &amp; Clerk, 27 Imperial Square, Cheltenham, Gloucestershire GL50 1RQ (GB).

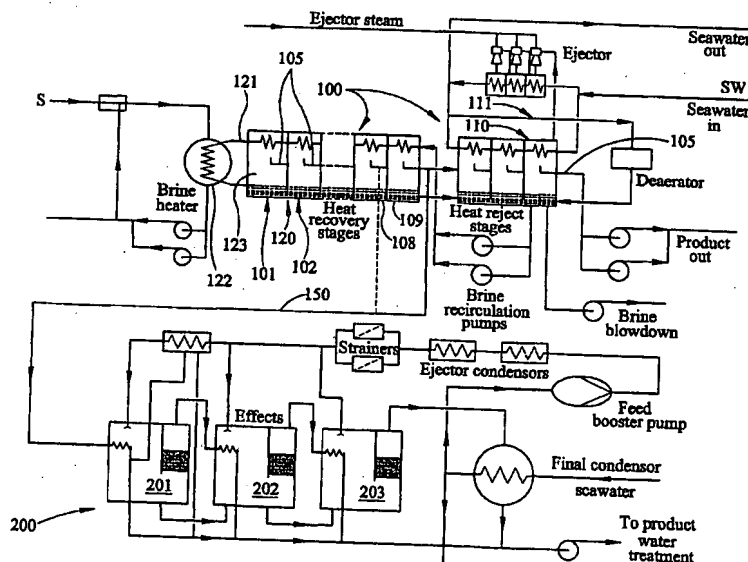
(84) Designated States (unless otherwise indicated, for every kind of regional protection available): ARIPO (BW, GH, GM, KE, LS, MW, MZ, NA, SD, SL, SZ, TZ, UG, ZM, ZW), Eurasian (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European (AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI, FR, GB, GR, HU, IE, IS, IT, LT, LU, LV, MC, NL, PL, PT, RO, SE, SI, SK, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).

Published:

— with international search report

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

(54) Title: MSF DISTILLATE DRIVEN DESALINATION PROCESS AND APPARATUS



(57) Abstract: A desalination process for the production of potable water comprising the steps of extracting at least one distillate stream (150) from at least one higher temperature stage (109) of an MSF separation process (100) and supplying said at least one distillate stream to at least one stage of a separation process (200) operating at a lower temperature than said higher temperature so as to maximise the use of sensible heat in said distillate stream by heat transfer in said at least one stage, to lower the external heat input of said at least one stage and of the process overall.

WO 2006/021796 A1

---

**MSF DISTILLATE DRIVEN DESALINATION PROCESS AND APPARATUS****Technical Field**

5           The invention relates to improvements in processes involving multiple stage flash distillation (MSF) generally and in particular the MSF distillation of seawater i.e. desalination to produce potable water, and relates advantageously to processes including MSF distillation of the kind in which a high top brine temperature is achievable (of the order of 120°C or more).

10

**Description of Related Art**

          The known conventional processes for the desalination of salt water to produce potable water include, for example, multistage flash distillation (MSF), multiple effect  
15   distillation (MED), reverse osmosis (RO) and vapour compression (VC) distillation. Each of these processes is a well established technology having its own unique characteristics and limitations. However each technology has an independent energy input stream. So far, no studies have been made and no process configurations have been studied or proposed relating to the interaction between MSF and MED or MSF and  
20   RO energy process streams taking advantage of the different operating temperature regimes to maximize overall production for a given energy input.

          The seawater distillate flow condensed in an MSF tube bundle is forced partly to re-flash when it is transferred to a subsequent stage in an evaporator operating at a  
25   lower pressure. The vapour generated by the distillate flashing is mixed with the vapour generated by the brine flashing and thus uses part of the installed heat transfer surface that part being therefore unavailable for the condensation of the flashing brine.

          With increasing stage number, the flow rate of distillate collected in the distillate  
30   trough increases, and so does the amount of distillate re-flashing. This phenomenon decreases the efficiency of the stage heat transfer mechanism by reducing the effective

amount of distillate generated by flashing brine, i.e. the ratio of reflash of distillate to flashing of brine increases.

It should be noted furthermore that the known arrangement of distillate trough  
5 collecting and transferring the distillate from the high to the low temperature stage of the MSF becomes increasingly cumbersome and takes space away from demisters and flashing brine release areas.

The 'heat reject' section of a typical MSF plant uses external seawater cooling to  
10 maintain low temperature in the bottom temperature stages.

In this heat reject section the installed heat transfer surface is used both to produce new distillate by condensation of flashing brine and to condense the distillate flashed. Therefore the efficiency of this section of the plant is lower than the heat  
15 recovery and typically over 18% of the heat transfer area is used to condense re-flashed distillate.

Multistage flash distillers are in common use worldwide for large scale desalination projects. Their performance depends on both the maximum brine  
20 temperature (top brine temperature or TBT) and the minimum brine temperature (bottom brine temperature or BBT) that can be used in the process. The higher the difference between the TBT and the BBT (the flashing range), the higher the plant productivity becomes. Modern conventional MSF plants operate at a top brine temperature ranging between 105 ° C and 112 ° C; and the brine and distillate  
25 temperature in the bottom stage of the heat recovery section varies between 65° and 50° and depends on the seawater cooling flow rate and temperature. An advanced MSF plant employing a combination of MSF and Nanofiltration technology allowing TBT to exceed 120° C (as disclosed in Awerbuch EP 1206414 (WO 0114256)) and this provides an even larger flashing range. The proposed invention relates to a  
30 modification to the MSF plant design which allows more brine from the MSF plant to flash in the heat rejection section of the evaporator and be condensed in the larger heat transfer surface made available for the condensation of brine.

---

As a consequence, the brine bottom temperature is lower.

By virtue of these two effects the proposed process modification allows an increase of the process productivity.

5

MED technology has been used for relatively small applications and operations at relatively lower temperatures. The design top temperature adopted for MED processes varies between 60°C and 70°C.

10 In sea water reverse osmosis (SWRO) process recovery, reverse osmosis ratio and energy consumption depend on the feed water temperature. The optimal temperature ranges from 30 °C to 35° C, with a technical limit of 40°C for standard membranes.

15 In the Middle East during the winter season seawater temperatures range from 18°C to 28°C. in North African areas the winter seawater temperature is even lower reaching 14°C to 12°C and never exceeding 28°C. Membrane recovery ratio is defined as the ratio between the membranes permeate and the feed water flow. The higher the recovery ratio the lower both the membrane capital and operating costs become. There  
20 are technical limitations existing today in standard seawater membranes which prevent operation of a reverse osmosis plant at a temperature above 39° C.

However the optimal membrane feed water ranges between 28 °C and 32 °C .  
At lower temperatures the membrane recovery ratio is low, therefore less permeate can  
25 be obtained from the membrane with higher energy consumption.

There is a great need for a process that combines the advantages of MSF with the other two technologies, MED and SWRO in order to improve the operating conditions, efficiency and yield of both; taking advantage of the difference in the  
30 operating temperature profile of each type of desalination system. The present invention makes available sensible heat from MSF distillate extracted stream at a

sufficiently high temperature to both pre-heat seawater RO feed and/or MED feed-water.

### Summary of the Invention

5

The present invention is directed to an improved process for desalinating salt water at optimal operating conditions by matching MED, RO or other processes, with MSF.

10

The present invention provides a desalination process for the production of potable water comprising the steps of;

a) extracting at least one distillate stream from at least one higher temperature stage of an MSF separation process and;

15

b) supplying said at least one distillate stream to at least one stage of a separation process operating at a lower temperature than said higher temperature so as to maximise the use of sensible heat in said distillate stream by heat transfer in said at least one stage, to lower the external heat input of said at least one stage and of the process overall.

20

In accordance with the invention, the energy associated with the distillate extracted from the last stages of the MSF heat recovery section is recovered in another power or desalination cycle (e.g. MED or RO) operating at lower temperature.

25

In particular the extraction of the distillate from the distillate trough in the last stages of the heat recovery section of the MSF brings about an improvement in the MSF overall performance as the heat reject section transfer surface is less burdened by distillate and may handle a large volume of flashing brine.

30

Preferably, said at least one stage is a stage in which feedwater to the MSF separation process is preheated by the said at least one stream.

Desirably said at least one stage is a stage of a second separation process.

Advantageously the second separation process is MED operating at lower temperature, which is, at least in part, thermally driven by heat extracted from said at least one distillate stream derived from MSF. Said at least one distillate stream may be flashed in a series of flash evaporation processes to provide heat by direct transfer  
5 from the brine to the MED process.

Where said second separation process is MED, said at least one distillate stream may be flashed to cool the distillate, and the fluid vapour is thermocompressed by ejectors to a high temperature and then input to a higher effect of the MED process.  
10

Also where said second separation process is MED, said at least one distillate stream may be subjected to a series of heat exchange steps in which heat is transferred from the distillate stream to the distillate of the MED.

15 As an alternative, the second separation process may be a reverse osmosis (RO) process in which the distillate stream from the MSF is used to preheat the seawater feed to the RO process.

At the same time the heat extracted from the MSF in the form of distillate can be  
20 utilized as an energy source for a lower temperature process such as the MED.

Particularly the distillate can be either used in a liquid form to feed the MED or it can be flashed and recompressed and input to the MED first stage.

25 The application of this invention to hybrid MSF/RO processes foresees the use of the extracted distillate to heat the seawater feed to the RO plant for example in winter season in order to obtain a higher recovery ratio from the RO membrane.

As a direct result, a number of advantages are realized which include both a  
30 more cost-efficient operation of MSF desalination and a reduction in the energy consumption of the MED or RO plants using the energy stream cascaded from the MSF.

It should be noted that the invention makes available energy from the MSF plant with a contemporary improvement of the MSF plant performances.

The distillate extraction system from the MSF involves other advantages especially in the apparatus/plant, in fact because the distillate trough in the heat rejection section can be substantially smaller, and/or a larger space can be made available to a demister. This space is particularly precious in the heat reject section which is operating under high vacuum, handles large volumes of vapour and this therefore results in high vapour velocities in the demisters.

10

These in turn are responsible for both loss of efficiency and high conductivity when flooding conditions occur. In this respect, if the larger demister space made available by the reduction of the distillate trough is considered, a further improvement in MSF plant performances can be achieved. The removal of distillate from multistage flash (MSF) stages provides the means to increase production of the desalination plants. The energy contained in the distillate, depending on the stage of removal of distillate, can be recovered by flashing to one or more appropriate multi-effect distillation process (MED) effect-cycle – or preheating the feed to another desalination process such as RO.

20 In the case of distillate removal from last stage of recovery section before the reject section, the heat flashed in the last stages is not at all beneficial, necessary or required for the MSF distillation process, but could be used to preheat feed to membrane processes, as proposed.

25 In general, heat of reflash distillate is condensing on heat transfer surfaces (HTS) and requires a tube area for condensation which could be used for condensing additional new vapour produced from flashing brine. The additional area, not occupied by a distillate collector channel, can be used to increase the area of demisters, particularly in lower stages of MSF.

30

The heat removed from MSF stages by taking distillate from MSF can be reflash to lower temperature of MED effects, both to provide sensible heat to preheat

---

feed in direct contact, or through feedwater heaters of MED.

The result of removal of distillate from all or some strategically located stages of MSF plant will provide additional output of distilled water of existing and future MSF plants. The heat contained and the thermal potential of the distillate is recovered by hybridization with MED, VC or RO processes. This allows maximisation of production, both in MSF, as well as increasing efficiency of other desalination processes. The preferred process is to remove distillate every few stages and transfer the available heat by flashing in MED flash tanks which provide vapour to preheat the feed in direct contact with spray sub-cooled feed, or provide steam-vapour to feedwater heater.

#### **Brief Description of the Drawings**

Fig. 1 is a schematic flow diagram of an integrated hybrid MSF - MED desalination process using a distillate stream from the high temperature stage of a MSF distillation as a direct feed to an MED process.

Fig. 2 is a schematic flow diagram illustrating a second, hybrid MSF - MED desalination process in which the distillate is flashed and the vapour fed to MED process.

Fig. 3 is a schematic flow diagram illustrating a third, fully integrated, MSF - MED desalination process using distillate from the MSF process and recycling brine and noncondensable gases to enhance the MED performance.

Fig. 4 is a schematic flow diagram illustrating a fourth, hybrid MSF - RO desalination process using distillate from the MSF plant to preheat the feed water to RO process.

30

Fig. 5 is a graph showing the percentage increase in distillate production against the distillate extraction.



### Description of the Preferred Embodiments

The prior art MSF desalination processes are significantly improved by the present invention. Having read and understood the features and principles of the invention as presently described and shown in the figures, an experienced engineer in designing, manufacturing and operating water desalination systems of the type contemplated by this invention would be able to practice the invention and realize its benefits.

According to one aspect of the invention, the improvement resides with the discovery that the extraction of the MSF distillate can be used to provide energy to another process cycle operating at a lower temperature. It has been discovered furthermore that the extraction brings about substantial improvements in the performance of MSF desalination plant from which the distillate is extracted. These improvements are not suggested by the prior art.

In each of the embodiments of Figures 1 to 4 there is provided a MSF shown generally as 100 which comprises heat reject stages 110 and heat recovery stages 120.

The principles of MSF distillation are simple. Sea water feed (SW) is pressurized and heated to the maximum plant temperature. When the heated liquid is discharged into a chamber 123 maintained slightly below the saturation vapour pressure of the liquid, a fraction of its water content flashes into steam. The flash steam is then stripped of suspended brine droplets as it passes through a mist eliminator and condenses on the exterior surface of heat transfer tubing. The condensed liquid drips into trays (105) as hot product water.

The unflashed brine enters a second chamber, or stage, where it flashes to steam at a lower temperature, thereby producing an additional quantity of product water. Simultaneously, the distillate from the first stage (101) passes to the distillate tray in the second stage and gives up some of its heat. The flash-cooling process is repeated

---

from stage to stage until both the cooled brine and the cooled distillate are finally discharged from the plant as blowdown brine and product water, respectively.

The recirculating brine (121) stream flowing through the interior of the tubes  
5 that condenses the vapour in each stage serves to remove the latent heat of  
condensation. In so doing, the recirculating brine is pre-heated, simultaneously  
recovering the energy of the condensing vapour. This portion of the multistage flash  
distillation plant is called the "heat recovery" section. The pre-heated brine is finally  
brought up to the maximum operating temperature in a brine heater (122) supplied with  
10 steam from an external source (S). The cool end of the plant, called the "heat  
rejection" section has the task to both remove the waste heat by external cooling  
seawater and produce distillate by condensing part of the remaining part-flashing brine  
from the heat recovery section. A fraction (111) of this cooling stream, branched  
downstream of the heat reject section, is pre-heated and becomes make-up water.

15

Specifically, with the present invention, by extracting a stream 150 of distillate  
in the last heat recovery stages 109 (and optionally 108 in broken line) of the MSF  
evaporator, MSF production increases without any substantial decrease in the  
performance ratio and therefore without any increased external steam requirement.

20

Furthermore, in apparatus for the process of new construction a larger space can  
be made available for demisters therefore allowing a further improvement in plant  
performance.

25

The energy of the distillate stream is used as an energy source for a distinct  
MED separator shown generally as 200 comprising a series of effects 201, 202, 203,

The use of distillate as a heat source for an MED process allows the MED to  
operate with very low supplied (external) heat consumption and increases the energy  
30 efficiency of the system.

It should be noted that in addition to the performance improvement, the invention grants some environmental benefits. As indicated in table 1 below, with the same seawater flow rate through the heat reject section both the bottom brine temperature (BBT) and the heat reject outlet temperature is lower. Alternatively the cooling water flow rate through the heat reject section can be reduced, or a combination of the two may be achieved. Both aspects bring about an improvement of the environmental impact.

Table 1 summarizes the advantages achieved by the present invention in the both the options of retrofitting the concept in an existing site or introducing it as a design feature for a new plant.

Table 1 : summary of invention benefits

EXISTING PLANT (retrofit)	NEW PLANT
Increase in MSF Distillate output without decrease in performance ratio.	Increase in MSF Distillate output and increase in plant performance ratio.
Extraction of a thermal stream usable in another process	Extraction of a thermal stream usable in another process
Modification of the internal distiller layout with possibility to increase demister/release areas and decrease distillate tray.	Optimization in internal distiller layout with possibility to increase demister/release area and decrease distillate tray.
Decrease in demisters velocity and increase in distillate purity. Protection of purity of the main distillate stream by removal before reject section. Reduction of parasitic losses	Decrease in demisters velocity and increase in distillate purity. Protection of purity of main distillate stream by removal before reject section
Reduction of brine bottom temperature	Reduction of brine bottom temperature
Possibility to reduce sea water consumption	Possibility to reduce seawater consumption

If the invention is retrofitted in an existing MSF plant there are unavoidable constraints given by the existing design which may prevent the increase of the demisters area. In this case as indicated in table 1 the plant output will increase. The plant

percentage increase is indicated in Figure 5 and Table 2. If the invention is applied to a new MSF plant the same may imply a redesign of the evaporator internal arrangement in the last stage of the heat reject section which makes available more space to demisters and therefore allows an increase in the performance ratio.

5

Table 2 shows a comparative analysis of a 5 MIGD (million Imperial gallon per day) 17 stages MSF plant operating under the same conditions of top brine temperature, seawater temperature and brine recirculation flow rate with the extraction of the distillate flow (in accordance with the invention) from the 14<sup>th</sup> stage.

10

TABLE 2

MSF PERFORMANCE WITH AND WITHOUT DISTILLATE  
EXTRACTION

PARAMETER	WITH DISTILLATE EXTRACTION	WITHOUT DISTILLATE EXTRACTION
TOP BRINE TEMPERATURE	110°C	110°C
BOTTOM BRINE TEMPERATURE	41.3 °C	42.4 °C
DISTILLATE FLOW	1157.95 Tons/hr	1174.7 Tons/hr
PERFORMANCE RATIO	7.46 (t/t)	7.45 (t/t)
STEAM DEMAND	155.27 (Tons/hr)	157.74 (Tons/hr)
ENERGY MADE AVAILABLE TO DOWNSTREAM CYCLE	61384 kJ/s	0

15

The desalination apparatus conceived includes distillate removal from MSF to be flashed in a tank to cool the distillate and the vapour flashed are thermo- compressed through ejectors to higher temperature entering higher stage of MSF

20

One of the benefits of the invented apparatus includes distillate removal from MSF to be flashed in a flashing tank to cool the distillate, and distillates and the flashed

vapour are condensed in a process operating at lower temperature to obtained a double distilled product of extremely high purity below .01 ppm TDS.

Figure 1 illustrates a basic flow diagram of an MSF – MED integrated system  
5 with an MED first effect heated up by distillate extracted from the MSF instead of condensing steam.

The MED plant is in all aspects similar to a conventional MED plant with the difference that the first effect is fed by distillate from the MSF instead of steam. The  
10 distillate is cooled in the first effect by transfer of heat to fresh seawater in the MED effect.

An alternative pattern is indicated in Figure 2 where MSF distillate is conveyed to a flashing tank and the vapour generated by distillate flashing is thermo compressed  
15 to the evaporator first stage.

The desalination apparatus conceived includes the heat transfer in a series of flashing tanks providing flashed vapour by direct contact from the distillate to the MED. The desalination apparatus according to the invention provides for the distillate  
20 removed from MSF to a flashing tank to cool the distillate and the flashed vapour are thermo- compressed by ejectors to a higher temperature before entering a higher effect of MED

An alternative desalination apparatus according to the invention provides for the  
25 heat transfer to be conducted in a series of heat exchangers between the MSF distillate and the distillate of MED

(a) A full integrated MED – MSF option is shown in Figure 3. According to one embodiment of the present invention three streams are extracted from MSF and  
30 conveyed to MED: distillate, un-condensable vent from first stage, brine blow down. Brine is used as feed water to the MED, and hot distillate is used instead of steam. The inventive step includes extraction of MSF brine streams to a MED

process by routing the brine extraction to a second process operating at lower temperature in order to utilize the sensible heat of the brine stream, In this case the invented desalination apparatus comprise of an apparatus for the heat transfer is a series of flashing tanks providing flashed vapour by direct contact from the brine to the MED. An alternative desalination apparatus according to the invention includes brine removed from MSF is flashed in a flashing tank to cool the distillate and the vapour flashed a re thermo- compressed by ejectors to higher temperature entering higher effect of MED Another alternative of the inventive apparatus provides for the heat transfer in a serious of heat exchangers between the brine of MSF and the feed of MED.

At the operating temperature of the MED plant the risk of precipitation of Magnesium hydroxide would be prevented from the injection in the stage of CO<sub>2</sub> from the MSF with the advantage that the MED plant will always be in cleaner conditions.

The operating configuration of Figure 4 illustrates a hybrid MSF/RO plant with RO feed water heated up by MSF distillate extracted as previously indicated.

According to one embodiment of the invention, the membrane feed water is heated up to 28- 30 degrees by the sensible heat of the distillate with the benefit of maintaining a higher permeate recovery ratio a lower specific power consumption and a more constant working temperature to the membrane inlet which is reflected in a longer membrane life.

The desalination apparatus according to this invention provides for the apparatus for the heat transfer is a series of flashing tanks providing flashed vapour by direct contact from the distillate to the RO feed. Alternative embodiment of this invention provides for distillate removal from MSF to be flashed in a flashing tank to cool the distillate and the vapour flashed are thermo- compressed by ejectors to higher temperature to heat the RO feed. Another alternative provides for desalination apparatus for the heat transfer to be heat exchangers between the MSF distillate and the RO feed.

---

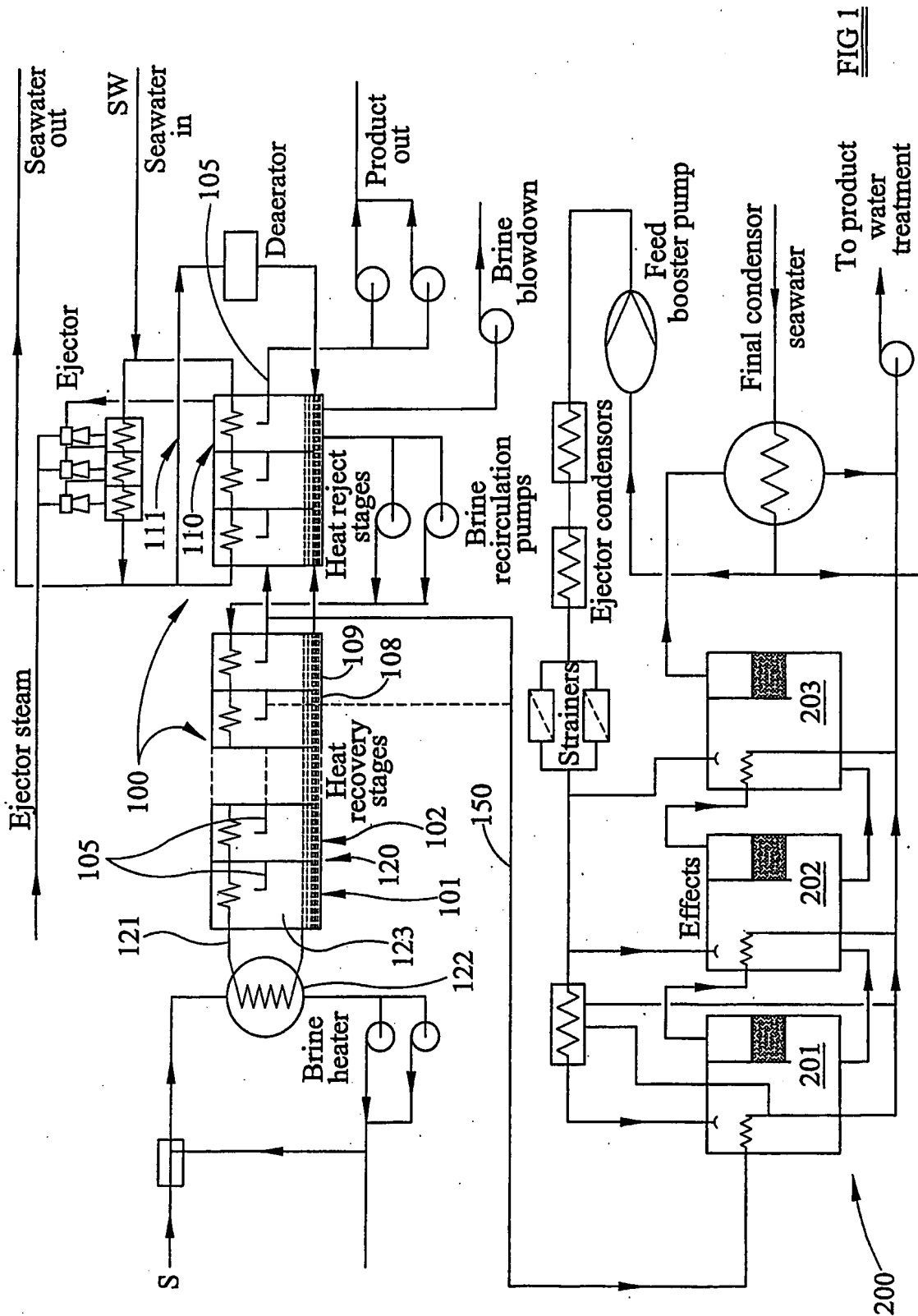
The graph shown in Figure 5 is based on a nominal 5 million imperial gallons per day (MIGD) throughput. With throughputs at present exceeding 15 MIGD the increase in output would be proportionally increased.

## CLAIMS

- 
1. A desalination process for the production of potable water comprising the steps of;
    - a) extracting at least one distillate stream (150) from at least one higher temperature stage (109) of an MSF separation process (100) and;
    - b) supplying said at least one distillate stream to at least one stage (201) of a separation process (200) operating at a lower temperature than said higher temperature so as to maximise the use of sensible heat in said distillate stream by heat transfer in said at least one stage, to lower the external heat input of said at least one stage and of the process overall.
  2. A desalination process as claimed in claim 1 in which said at least one stage is a stage in which feedwater to the MSF separation process is preheated by the said at least one stream.
  3. A desalination process as claimed in claim 1 or claim 2 in which said at least one stage (201) is a stage of a second separation process (200).
  4. The desalination process as claimed in claim 3 in which the second separation process is MED (200) operating at lower temperature, which is, at least in part, thermally driven by heat extracted from said at least one distillate stream derived from MSF.
  5. A desalination process as claimed in claim 4 in which said at least one distillate stream is flashed in a series of flash evaporation processes (Fig 2) to provide heat by direct transfer from the brine to the MED process.
  6. A desalination process as claimed in claim 4 or claim 5 in which said at least one distillate stream is flashed to cool the distillate, and the fluid vapour is thermocompressed by ejectors (Fig 2) to a high temperature and then input to a higher effect of the MED process.



- 
7. A desalination process as claimed in claim 4 or claim 5 in which said at least one distillate stream is subjected to a series of heat exchange steps in which heat is transferred from the distillate stream to the distillate of the MED.
  8. A desalination process as claimed in claim 3 in which the second separation process is a reverse osmosis (RO) process in which the distillate stream from the MSF is used to preheat the seawater feed to the RO process.
  9. A desalination process as claimed in any preceding claim in which the heat extracted from the MSF in the form of distillate is utilized as an energy source for a lower temperature process such as the MED.
  10. A desalination process as claimed in claim 9 in which the distillate is used in a liquid form to feed the MED.
  11. A desalination process as claimed in claim 9 in which the distillate is flashed and recompressed and input to the MED first stage.



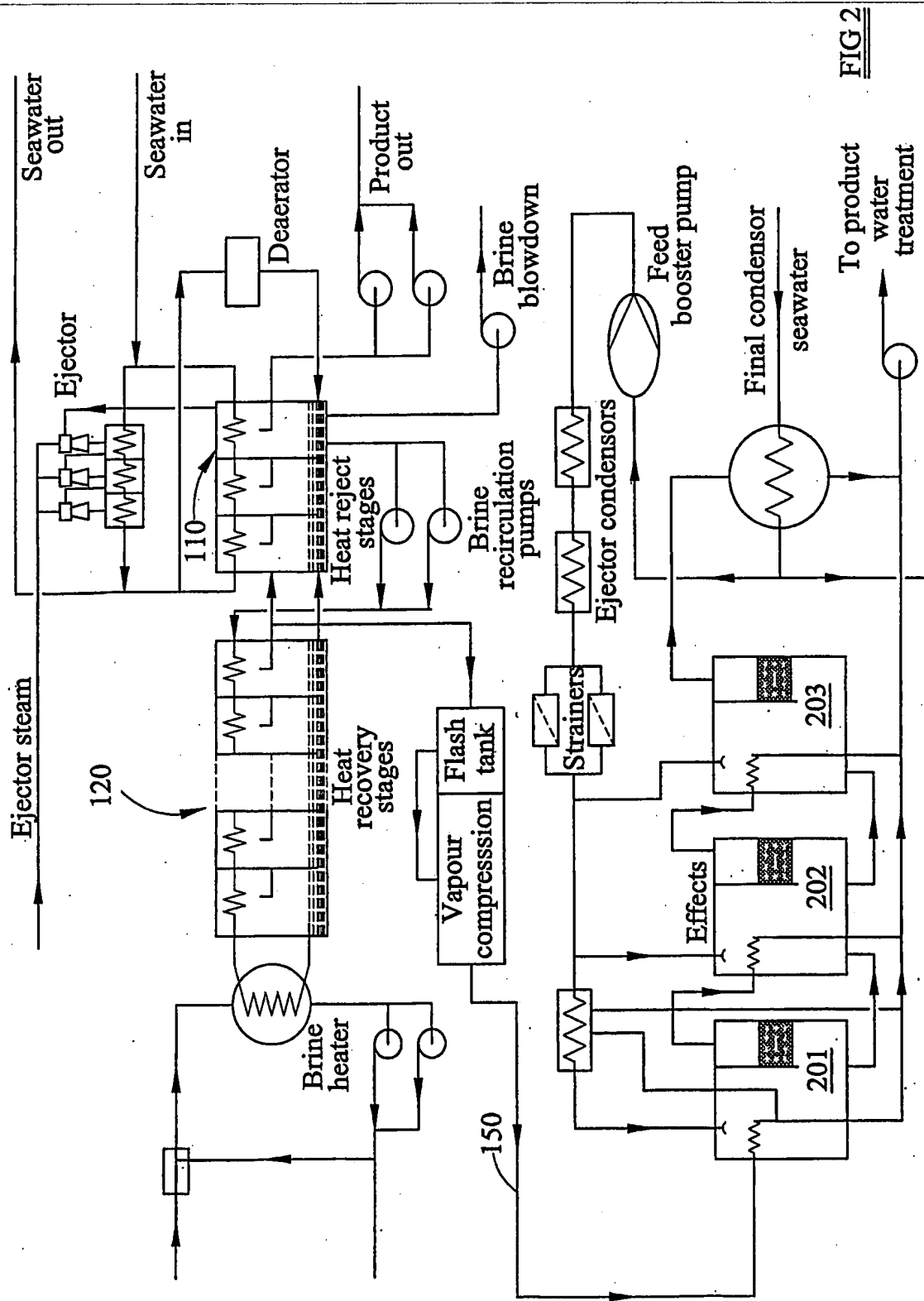


FIG 2



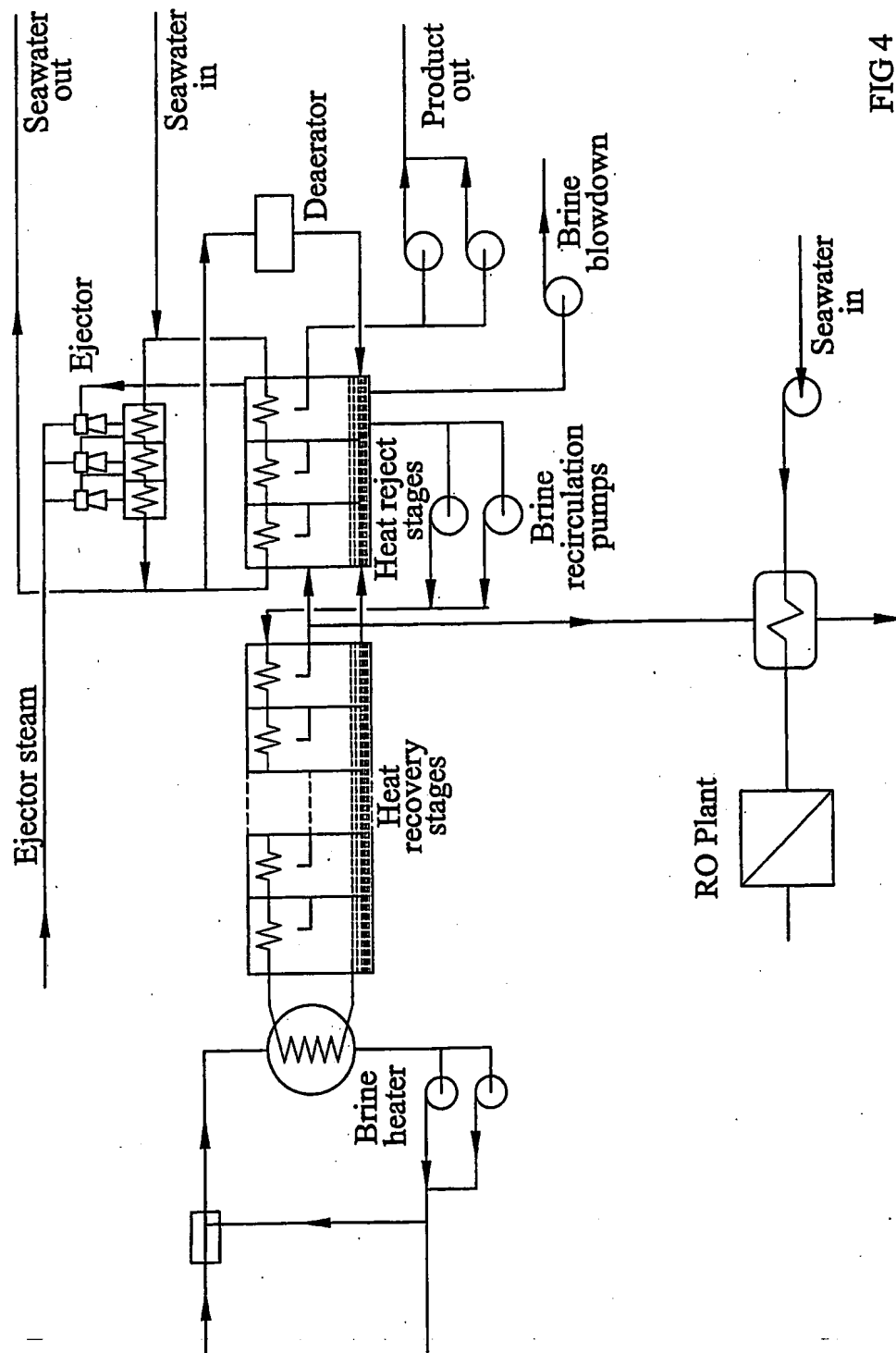


FIG 4

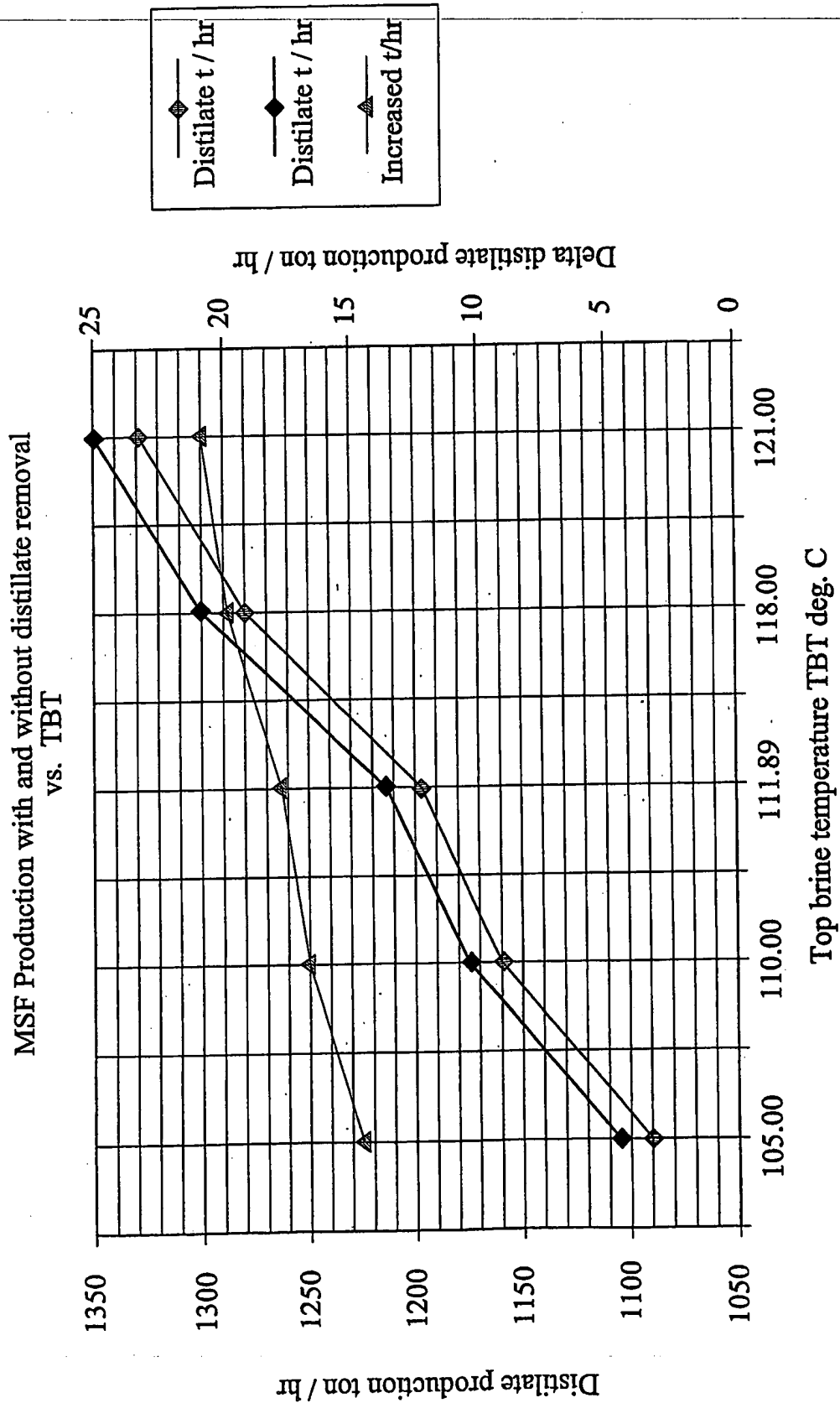


FIG 5

## INTERNATIONAL SEARCH REPORT

Int. Patent Application No.  
P. GB2005/003329

A. CLASSIFICATION OF SUBJECT MATTER B01D3/06 C02F1/06		
According to International Patent Classification (IPC) or to both national classification and IPC		
B. FIELDS SEARCHED		
Minimum documentation searched (classification system followed by classification symbols) C02F B01D		
Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched		
Electronic data base consulted during the International search (name of data base and, where practical, search terms used) EPO-Internal, WPI Data, PAJ		
C. DOCUMENTS CONSIDERED TO BE RELEVANT		
Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	DE 39 38 012 A1 (SERCK COMO GMBH, 2000 HAMBURG, DE) 16 May 1991 (1991-05-16) the whole document	1-11
A	US 3 489 654 A (PAUL L. GEIRINGER) 13 January 1970 (1970-01-13) the whole document	1-11
A	US 6 508 936 B1 (HASSAN ATA M) 21 January 2003 (2003-01-21) the whole document	1-11
-/-		
<input checked="" type="checkbox"/> Further documents are listed in the continuation of box C. <input checked="" type="checkbox"/> Patent family members are listed in annex.		
* Special categories of cited documents : "A" document defining the general state of the art which is not considered to be of particular relevance "E" earlier document but published on or after the international filing date "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) "O" document referring to an oral disclosure, use, exhibition or other means "P" document published prior to the international filing date but later than the priority date claimed "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention "X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone "Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art "Z" document member of the same patent family		
Date of the actual completion of the international search  11 November 2005		Date of mailing of the international search report  22/11/2005
Name and mailing address of the ISA European Patent Office, P.B. 5818 Patentlaan 2 NL - 2280 HV Rijswijk Tel. (+31-70) 340-2040, Tx. 31 651 epo nl, Fax: (+31-70) 340-3016		Authorized officer  Lieb1g, T

## INTERNATIONAL SEARCH REPORT

International Application No  
6B2005/003329

C. (Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT		
Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	LUDWIG H: "Hybrid systems in seawater desalination-practical design aspects, present status and development perspectives" DESALINATION, ELSEVIER, AMSTERDAM, NL, vol. 164, no. 1, 25 March 2004 (2004-03-25), pages 1-18, XP004513008 ISSN: 0011-9164 the whole document	1-11



## INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PC B2005/003329

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
DE 3938012	A1	16-05-1991	NONE
US 3489654	A	13-01-1970	NONE
US 6508936	B1	21-01-2003	AU 9584998 A 23-04-1999
		EP 1019325 A1 19-07-2000	
		WO 9916714 A1 08-04-1999	

**This Page is Inserted by IFW Indexing and Scanning  
Operations and is not part of the Official Record**

**BEST AVAILABLE IMAGES**

Defective images within this document are accurate representations of the original documents submitted by the applicant.

Defects in the images include but are not limited to the items checked:

- ☐ **BLACK BORDERS**
- ☐ **IMAGE CUT OFF AT TOP, BOTTOM OR SIDES**
- ☐ **FADED TEXT OR DRAWING**
- ☐ **BLURRED OR ILLEGIBLE TEXT OR DRAWING**
- ☐ **SKEWED/SLANTED IMAGES**
- ☐ **COLOR OR BLACK AND WHITE PHOTOGRAPHS**
- ☐ **GRAY SCALE DOCUMENTS**
- ☒ **LINES OR MARKS ON ORIGINAL DOCUMENT**
- ☐ **REFERENCE(S) OR EXHIBIT(S) SUBMITTED ARE POOR QUALITY**
- ☐ **OTHER:**

**IMAGES ARE BEST AVAILABLE COPY.**

**As rescanning these documents will not correct the image problems checked, please do not report these problems to the IFW Image Problem Mailbox.**